AMENDMENT TO THE CLAIMS:

The following claim set replaces all prior versions, and listings, of claims in the application:

- 1. (currently amended) Process for purifying caprolactam, said process comprising
- (a) subjecting the caprolactam to a hydrogenation by treating the caprolactam with hydrogen in the presence of a heterogeneous nickel containing hydrogenation catalyst, and
- (b) continuously distilling at least a portion of the hydrogenated caprolactam in a distillation column which , characterized in that the distillation column contains nickel in an amount sufficiently low such that $\Delta PAN_{Ni} \leq 3$ during a period of at least 3 months, wherein

 $\Delta PAN_{Ni} = \Delta PAN - \Delta PAN_{Ni=0}$,

 ΔPAN = increase of the PAN number of caprolactam during distilling, $\Delta PAN_{Ni=0}$ = increase of the PAN number of caprolactam during distilling under the same conditions in a distillation column free of nickel.

- 2. (original) Process according to claim 1, wherein the distillation column contains nickel in an amount sufficiently low such that $\Delta PAN \leq 3$.
- 3. (original) Process according to claim 1, wherein the distillation column contains nickel in an amount sufficiently low such that $\Delta PAN_{Ni} \leq 2$.
- 4. (original) Process according to claim 3, wherein the distillation column contains nickel in an amount sufficiently low such that $\Delta PAN_{Ni} \leq 1$.
 - 5. (canceled)

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- 6. (previously presented) Process according to claim 1, wherein the process further comprises, prior to said distilling, separating nickel from hydrogenated caprolactam.
- 7. (original) Process according to claim 6, wherein said separating is effected using filtration.
- 8. (previously presented) Process according to claim 1, wherein the nickel containing hydrogenation catalyst is a fixed bed catalyst.
- 9. (previously presented) Process according to claim 1, wherein the hydrogenation is a slurry phase hydrogenation wherein nickel containing hydrogenation catalyst particles are suspended in the caprolactam to be hydrogenated.
- 10. (original) Process according to claim 9, wherein after said hydrogenation the catalyst particles are separated from the hydrogenated caprolactam.
- 11. (previously presented) Process according to claim 6, wherein said separating of nickel from hydrogenated caprolactam is carried out after said separating of catalyst particles from the hydrogenated caprolactam.
- 12. (previously presented) Process according to claim 1, wherein the amount of nickel in the hydrogenated caprolactam entering said distilling is less than 10 ppm.
- 13. (original) Process according to claim 12, wherein the amount of nickel in the hydrogenated caprolactam entering said distilling is less than 1 ppm.
- 14. (previously presented) Process according to claim 1, wherein said distilling is effected in a distillation column having a bottom temperature of between 110 and 180°C.

- 15. (currently amended) Process according to claim 1, wherein said distilling is effected in a distillation column in which the caprolactam of the hydrogenated caprolactam has a residence time higher than 5 minutes.
- 16. (previously presented) Process according to claim 1, wherein said distilling is performed continuously and $\Delta PAN_{Ni} \leq 3$ during a period of at least 6 months.
- 17. (previously presented) Process according to claim 1, wherein the amount of nickel in the hydrogenated caprolactam entering said distilling is sufficiently low such that $\Delta PAN_{Ni} \leq 3$ during a period of at least 6 months.
- 18. (previously presented) Process according to claim 1, wherein water is separated from the hydrogenated caprolactam prior to said distilling.
- 19. (previously presented) Process according to claim 1, wherein separating nickel from hydrogenated caprolactam is effected after separating of water and prior to said distilling.
- 20. (previously presented) Process according to claim 1, wherein the caprolactam entering said hydrogenation is obtained by rearrangement of cyclohexanone oxime with sulfuric acid or oleum.
- 21. (currently amended) Process for purifying caprolactam <u>which comprises the</u> <u>steps of:</u> , for instance according to claim 1, said process comprising:
 - (a) subjecting the caprolactam to a hydrogenation by treating the caprolactam with hydrogen in the presence of a heterogeneous nickel containing hydrogenation catalyst; and
 - (b) <u>continuously</u> distilling at least a portion of the hydrogenated caprolactam in a distillation column , <u>characterized in that which contains nickel in an amount sufficiently low such that $\Delta PAN_{Ni} \leq 3$ during a period of at least 3 months, wherein</u>

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 $\Delta PAN_{Ni} = \Delta PAN - \Delta PAN_{Ni=0}$

 ΔPAN = increase of the PAN number of caprolactam during distilling, $\Delta PAN_{Ni=0}$ = increase of the PAN number of caprolactam during distilling under the same conditions in a distillation column free of nickel, and wherein

- distilling according to step (b) is continued during a period of at last 3

 months, and wherein the amount of nickel in the hydrogenated caprolactam entering said distilling has a nickel content which is less than 50 ppm, preferably less than 10 ppm, more preferably less than 1 ppm, even more preferably less than 500 ppb and even more preferably less than 100 ppb.
- 22. (New) Process according to claim 21, wherein the nickel content in the hydrogenated caprolactam entering said distilling is less than 10 ppm.
- 23. (New) Process according to claim 21, wherein the nickel content in the hydrogenated caprolactam entering said distilling is less than 1 ppm.
- 24. (New) Process according to claim 21, wherein the nickel content in the hydrogenated caprolactam entering said distilling is less than 500 ppb.
- 25. (New) Process according to claim 21, wherein the nickel content in the hydrogenated caprolactam entering said distilling is less than 100 ppb.
- 26. (New) Process according to claim 21, wherein distilling according to step (b) is continued during a period of at least 6 months.